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## Biochemical Engineering

### Exercise Session 6

#### 1) Constant feed fed-batch

In a fed-batch culture of *Escherichia coli* operating with feed of a glucose solution, values of the following parameters are given at time  $t = 2$  h, when the system is at quasi-steady state.

$$\begin{array}{ll} V = 1000 \text{ mL} & dV/dt = 200 \text{ mL h}^{-1} \\ s_0 = 100 \text{ g glucose L}^{-1} & \mu_{\max} = 0.3 \text{ h}^{-1} \\ K_s = 0.1 \text{ g glucose L}^{-1} & Y_{X/S} = 0.5 \text{ g cells (g glucose)}^{-1} \\ X_0 = 30 \text{ g (total = } x_0^i) \end{array}$$

- Find  $V_0$  (the initial volume of the culture)
- Determine the concentration of growth-limiting substrate in the vessel at quasi-steady state at  $t = 2$  h.
- Determine the concentration and total amount of biomass in the vessel at  $t = 2$  h (at quasi-steady state)
- If  $q_p = 0.2 \text{ g product (g cells)}^{-1} \text{ h}^{-1}$ ,  $p_0 = 0$ , determine the concentration of product in the vessel at  $t = 2$  h.

#### 2) Design of a multi-phase fed-batch for the production of lipase

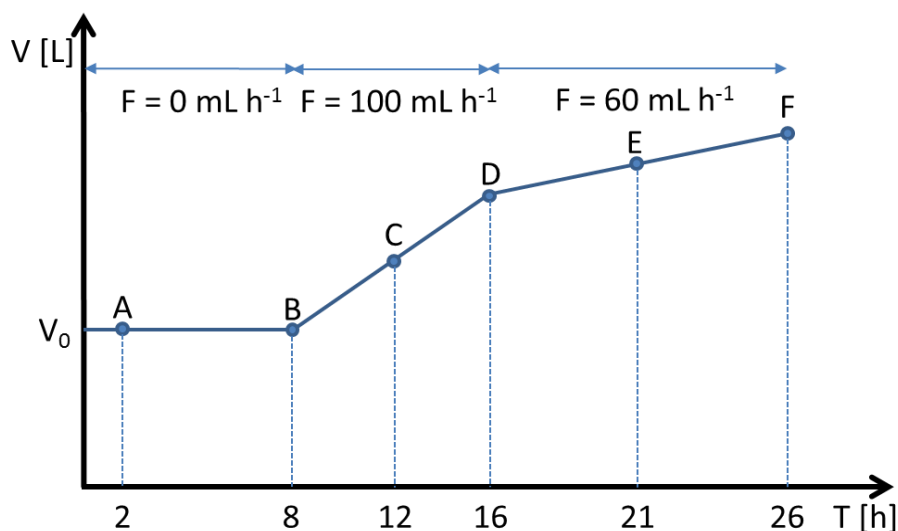
A fed-batch for the production of a lipase is carried out with a recombinant strain *Yarrowia lipolytica* (see also figure below):

Phase 1: Batch on glucose ( $s_0$  (Glucose) =  $6 \text{ g L}^{-1}$ )

Phase 2: Fed-batch on glycerol Feed1  $s_0$  (Glyc) =  $1260 \text{ g L}^{-1}$

Phase 3: Fed-batch on lactose with Feed2  $s_0$  (Lact) =  $500 \text{ g L}^{-1}$ .

Inoculum batch :  $X_0 = 0.1 \text{ g}$



**Questions:**

a) Calculate the culture volume of the bioreactor at times B, C, D, E, and F

Note:  $V_0 = A = 2.0 \text{ L}$

B : ..... C : ..... D : ..... E : ..... F : .....

b) Calculate the dilution rates for the time points A, C, and E.

A: .....; C: .....; E: .....

c) Calculate the total biomasses for the time points B, D, and F.

Note:  $Y_{X/\text{Gluc}} = 0.5 \text{ g g}^{-1}$ ,  $Y_{X/\text{Glyc}} = 0.1 \text{ g g}^{-1}$ ,  $Y_{X/\text{Lact}} = 0.3 \text{ g g}^{-1}$

B: .....; D: .....; F: .....

d) Calculate the concentration of lipase at the end of the fed-batch (time point F).

Note:  $Y_{\text{Lipase}/X} (\text{Glucose}) = 0 \text{ g g}^{-1}$ ,  $Y_{\text{Lipase}/X} (\text{Glyc}) = 0.01 \text{ g g}^{-1}$ , on lactate:  $Y_{\text{Lipase}/X} = 0.5 \text{ g g}^{-1}$

F: .....

e) Calculate volumetric productivity of lipase and of the biomass for the *whole* bioprocess (time point F).

F: .....

**3) Different feed profiles**

Please complement the following figures with the trends you are expecting for the respective parameters for the following feed conditions:

1) Exponential feed; 2) Pulsed feed; 3) Constant feed

Note: Dashed line represents end of batch culture

